Statement of Basis Air Pollution Control Draft Title V Permit to Operate G&K Services, Inc. – Green Bay Permit No. V-ON-5500900021-2014-01

The purpose of this document is to set forth the legal and factual basis for permit conditions, including references to applicable provisions of the Clean Air Act (CAA or Act) and implementing regulations. This document also gives the derivation of conditions as required by 40 C.F.R. § 71.11(b).

1. GENERAL INFORMATION

a. Applicant and Stationary Source Information

| Owner | Source (SIC Code: 7218) |
|-----------------------------|------------------------------|
| G&K Services, Inc. | G&K Services, Inc.—Green Bay |
| 5995 Opus Parkway | 800 Isbell Street |
| Minnetonka, Minnesota 55343 | Green Bay, Wisconsin 54303 |

| Responsible Official | Facility Contact |
|-----------------------------|---------------------------------|
| Steve Botts: (952) 912-5500 | Douglas Krysiak: (920) 497-2509 |

b. Facility Description

G&K Services cleans and reconditions soiled industrial textiles such as towels, coveralls, uniforms, and other items for industrial customers. G&K Services operates five indoor-vented industrial washing machines, four stack-vented industrial washing machines, six natural gas-burning industrial dryers, a natural gas-fired steam tunnel, a 10.46 MMBTU/hr natural gas-fired boiler, and other processes, such as textile sorting activities and comfort heating.

G&K Services' customers include businesses in the printing and woodworking industries as well as automotive shops. These businesses send their soiled industrial towels to G&K Services to be washed. The soiled industrial towels from these customers typically contain volatile organic compounds (VOCs) and hazardous air pollutants (HAPs) that may be emitted from the facility as the towels are washed. Soiled industrial towels from other businesses and industry groups generally do not contain VOCs and HAPs.

G&K Services classifies the soiled industrial towels into three categories based on the towel's source. The first category, soiled print towels or "inkers," includes soiled industrial towels from printing, woodworking, wood finishing, and other facilities which return towels containing VOCs. The second category, soiled shop towels, includes towels from automotive shops and other similar operations which return

towels containing VOCs, oil, and/or grease. The third category includes towels and textiles from other sources that do not use materials containing VOCs or HAPs.

G&K counts and sorts soiled industrial towels, and launders them using a conventional industrial (aqueous) washing step and a drying step. The washing process consists of loading soiled textiles into an industrial washer and adding water, detergent, and other cleaning additives. The soiled textiles proceed through a washing stage, wash water draining stage, rinsing stage, and a final draining stage. Once washed, the textiles are then transferred to an industrial dryer for drying.

c. Area Classification

G&K Services Inc.—Green Bay is located within the exterior boundaries of the Oneida Tribe of Indians of Wisconsin's tribal reservation in Green Bay, Wisconsin. The EPA is responsible for issuing and enforcing any air quality permits for the source until the Tribe or State has EPA approval to do so.

The facility is located in Brown County, which is designated attainment with National Ambient Air Quality Standards for all criteria pollutants.

d. Title V Major Source Status

The facility has the potential to emit (PTE) more than 100 tons of VOC, particulate matter smaller than 10 microns (PM_{10}), and particulate matter smaller than 2.5 microns ($PM_{2.5}$) per year. Therefore, the facility is a major Title V source and must obtain a Title V permit.

e. Permit History

On February 13, 2013, G&K Services contacted EPA Region 5 to discuss the permitting status of its Green Bay facility. The facility is located within the Oneida Tribe of Indians of Wisconsin's reservation. As a result, EPA is the permitting authority for this facility.

Prior to the issuance of this permit, the facility operated according to the requirements of operating permits issued by the Wisconsin Department of Natural Resources (WDNR). Because WDNR did not have authority to issue Title V operating permits for the G&K Services – Green Bay facility, the operating permits issued by WDNR are not valid. However, these permits are listed below for reference:

- March 25, 2004: WDNR issued an initial Title V operating permit, permit number 405028690-P01, to G&K Services.
- December 21, 2007: WDNR issued permit modification 405028690-P02.

- March 16, 2009: WDNR issued a Title V permit renewal, permit number 405028690-P10, to G&K Services.
- February 25, 2010: WDNR issued permit modification 405028690-P11.
- July 11, 2011: WDNR issued permit modification 405028690-P12.
- May 17, 2013: WDNR issued permit modification 405028690-P13.

The current permit will be issued based on information provided in the following applications and follow-up information:

- June 14, 2013: G&K Services, Inc. application for an initial Part 71 permit.
- July 17, 2013: G&K Services, Inc., additional information explaining the calculation of emissions in its initial permit application.

2. PROCESS DESCRIPTION

a. Summary

G&K Services is an existing facility located at 800 Isbell Street in Green Bay, Wisconsin. The facility is physically located within the exterior boundaries of the Oneida Tribe of Indians of Wisconsin's reservation. Since the facility is located within the exterior boundary of an Indian reservation, EPA is the permitting authority responsible for issuing and enforcing air permits issued to G&K Services.

The facility operates the following emission units:

i. Process P01 – Industrial Washers Venting Indoors

| Emission | EU ID | Unit | Exhaust |
|--------------------------------|-------|----------------------------|---------|
| Unit | | Description | Stack |
| Jensen #3 | P36 | Industrial Washing Machine | Indoors |
| Braun #4 | P37 | Industrial Washing Machine | Indoors |
| Ellis Split Pocket #5 | P38 | Industrial Washing Machine | Indoors |
| Ellis Split Pocket #6 | P39 | Industrial Washing Machine | Indoors |
| Unimac #1 | P40 | Industrial Washing Machine | Indoors |
| Jensen L-Tron Washer/Extractor | P37 | Proposed replacement for | Indoors |
| Model 450 OPT-H | | Braun #4 | |

ii. Process P02 – Industrial Washers Venting to Stack S34

| Emission | EU ID | Unit | Exhaust |
|-----------|-------|----------------------------|---------|
| Unit | | Description | Stack |
| Jensen #1 | P34 | Industrial Washing Machine | S34 |
| Jensen #2 | P35 | Industrial Washing Machine | S34 |
| Unimac #2 | P25 | Industrial Washing Machine | S34 |
| Unimac #3 | P18 | Industrial Washing Machine | S34 |

iii. Process P03 – Industrial Dryers Burning Natural Gas

| Emission | EU ID | Unit | Heat Input | Exhaust |
|----------------------|-------|--------------------------|------------|---------|
| Unit | | Description | Rate | Stack |
| · | | | (MMBTU/hr) | |
| Challenge #3 | P08 | Industrial Dryer | 2.75 | S08 |
| Challenge #4 | P09 | Industrial Dryer | 2.75 | S09 |
| American #1 | P30 | Industrial Dryer | 3.5 | S30 |
| American #2 | P31 | Industrial Dryer | 3.5 | S31 |
| Cissell #1 | P05 | Industrial Dryer | 0.25 | S06 |
| Cissell #2 | P06 | Industrial Dryer | 0.25 | S07 |
| Jensen DTX 800 Dryer | P30 | Proposed replacement for | 2.5 | S30 |
| #1 | | American #1 | | |
| Jensen DTX 800 Dryer | P31 | Proposed replacement for | 2.5 | S31 |
| #2 | | American #2 | | |
| WashTech DR-80 | P05 | Proposed replacement for | 0.25 | S06 |
| Dryer | | Cissell #1 | | |

iv. Boiler B01 – 10.46 MMBTU Natural Gas-fired Boiler

| Emission | Unit | Burner Rating | Exhaust |
|------------|--------------------------|---------------|---------|
| Unit | Description | (MMBTU) | Stack |
| Boiler B01 | Natural gas-fired boiler | 10.46 | S01 |

v. Steam Tunnel

| Emission | Unit | Burner Rating |
|---------------------------|---------------------------|---------------|
| Unit | Description | (MMBTU/hr) |
| Leonard 24 foot Steam | Steam Tunnel Dryer | 0.8 |
| Tunnel | | |
| Leonard Automatics | Proposed steam tunnel | 3.0 |
| Model VPT24 Steam | replacing Leonard 24 foot | |
| Tunnel or a similar unit | steam tunnel | |
| with a capacity rating up | | |
| to 3.0 MMBTU/hr | | |

b. Insignificant Activities

The facility has the following insignificant activities as listed in 40 C.F.R. § 71.5(c)(11)(i):

- Mobile sources, such as forktrucks used for material transport
- HVAC units used for human comfort
- Office activities
- Janitorial services and consumer use of janitorial products.

The facility identified in its permit application the following emission units as insignificant activities based on insignificant emissions of regulated air pollutants and hazardous air pollutant pursuant to 40 C.F.R. § 71.5(c)(11)(ii):

- Continuous Roll Towel Machine
- Textile sorting and counting area
- Wastewater treatment/handling
- Boiler and HVAC maintenance
- Demineralization/Oxygen scavenging of Boiler Water
- Fire Control Equipment
- Maintenance of grounds, equipment, and buildings
- Purging of natural gas lines
- Sanitary sewer and plumbing venting.

c. Potential Emissions

Emission factors used to determine HAP and VOC PTE were determined through stack testing at the facility and other similar facilities owned by G&K Services, Inc. Emission factors listed for natural gas combustion units in AP-42, Fifth Edition, were used for determining the PTE of natural gas-fired emission units. Particulate matter (PM) emission factors were calculated using the available exhaust particulate matter loading, exhaust temperatures, and exhaust flow rates. It is assumed that the emissions of PM₁₀ and PM_{2.5} are equivalent to the PM emissions for the facility since separate PM₁₀ and PM_{2.5} emission factors are unavailable. This is a conservative estimate of potential PM₁₀ and PM_{2.5} emissions since all fractions of particulate matter are assumed to be emitted at the PM emission rate.

Calculations and the method used to calculate the emission potentials are included in spreadsheets as attachments to this statement of basis. The tables in this section represent the facility-wide potential to emit.

For the existing emission units at the facility, the PTE after federally-enforceable limits and controls are included in the table below. The figures are presented in tons per year.

| | Facility- | wide Pote | ential to l | Emit, Be | efore Mo | | n (tons j | per year) | |
|-------|-----------|-----------|-------------|----------|----------|-------|-----------|-----------|--------------|
| PM | PM_{10} | TN X / | × 7 6 | SO_2 | CO | VOC | Lead | Single | Total HAP |
| 205.2 | 205.2 | 205.2 | 25.7 | 0.1 | 12.7 | 122.5 | 0 | 8.4 | 21.2 |

Construction permit SYN-ON-55000900021-2014-01 authorized the replacement of several units at the facility. The following table gives the facility-wide potential to emit after all federally-enforceable limits and controls and after all authorized emission unit replacements are completed. The figures are presented in tons per year.

| | | wide Pot | ential to | Emit, A | | dification | ı (tons p | er year) | |
|-----------|-----------|----------|-----------|-----------------|------|------------|-----------|----------|-------|
| PM 1 | PM_{10} | PIVI2.5 | | SO ₂ | CO | VOC | Lead | Single | Total |
| | | | | | | | | HAP | HAP |
| 195.4 1 | 195.4 | 195.4 | 25.8 | 0.1 | 12.8 | 122.5 | 0 | 8.4 | 21.2 |

d. Actual Emissions

G&K Services is an existing facility operating pursuant to the operating permit erroneously issued by WDNR. As a result of a condition in that permit, the facility submits an annual emission inventory to WDNR. Although the permits were issued by WDNR, EPA has included as a part of the record for this permitting action the emissions inventory from 2012. Actual VOC, highest single HAP, and total HAP emissions for calendar year 2012 are included in the table below.

| VOC | HAP – Toluene | Total HAPs |
|------|---------------|------------|
| 57.1 | 4.12 | 9.2 |

Actual emissions for calendar year 2012 for all other pollutants are included in the table below. Figures are presented in tons.

| PM | PM_{10} | | | SO_2 | CO | Lead |
|------|-----------|------|------|--------|------|------|
| 2.99 | 2.99 | 2.99 | 1.79 | 0.01 | 0.88 | 0.02 |

3. APPLICABLE REQUIREMENTS

a. Title V Permitting

In accordance with 40 C.F.R. § 71.3(a)(1), all major stationary sources are required to obtain a Title V operating permit. "Major source" is defined at 40 C.F.R. § 71.2 as any stationary source belonging to a single major industrial grouping that directly emits or has the potential to emit 100 tons per year or more of any criteria pollutant. Since G&K Services' Green Bay facility has the potential to emit more than 100 tons per year of VOC, PM₁₀, and PM_{2.5}, it is a major stationary source subject to Title V.

b. Construction Permits

This Title V permit incorporates the conditions from the following construction permit issued pursuant to the federal minor new source review program in Indian country, codified at 40 C.F.R. §§ 49.151-161:

• After-the-Fact Synthetic Minor Air Quality Construction Permit, permit number SYN-ON-5500900021-2014-01.

c. New Source Performance Standards (NSPS)

G&K Services operates a 10.46 MMBTU natural gas-fired industrial boiler installed in 1982. This boiler is not subject to 40 C.F.R. Part 60, Subpart D, Da, or Db because it burns natural gas as its only fuel and has a capacity smaller than 100 MMBTU/hr. This boiler is not subject to 40 C.F.R. Part 60, Subpart Dc because it was constructed prior to June 9, 1989 and has not been modified or reconstructed since initial installation.

There currently are no new source performance standards for industrial washing machines, dryers, or steam tunnels.

d. National Emission Standards for Hazardous Air Pollutants (NESHAP)

G&K Services has requested federally-enforceable HAP emission limits designed to limit the source to no more than 8.4 tons per year of any single HAP and no more than 21.2 tons per year of total HAPs. As a result, G&K Services will be considered an area source for HAP emissions. Since G&K Services is an area source for HAP emissions, the facility is not subject to any major source NESHAPs.

G&K Services is not subject to 40 C.F.R. Part 63, Subpart JJJJJ: National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers Area Sources, because the boiler is a natural gas-fired boiler as defined at 40 C.F.R. § 63.11237. Pursuant to 40 C.F.R. § 63.11195(e), gas-fired boilers, as defined at 40 C.F.R. § 63.11237, are not subject to Subpart JJJJJJ.

Emission Overview for G&K Services, Inc. -- Green Bay

| | PTE Before Modification (After Enforceable Limits) | | | | | | | | | |
|-----------------------------|--|----------|----------|---------|----------|----------|-------|-------------|------------------------|------------|
| Process or Emission Unit | PM | PM10 | PM2.5 | NOx | SO2 | со | VOC* | Lead | Highest Single HAP* | Total HAP* |
| Boiler B01 | 0.341365 | 0.341365 | 0.341365 | 7.6358 | 0.02695 | 3.772984 | | 2.24582E-05 | | |
| Process P01 | 0 | 0 | 0 | 0 | 0 | 0 | | 0 0 | | |
| Process P02 | 9.984731 | 9.984731 | 9.984731 | 0 | 00 | 0 | 122.5 | | 0.4 | 21.2 |
| Process P03 | 171.2868 | 171.2868 | 171.2868 | 9.49 | 0.033494 | 4.689176 | 122.5 | 2.79118E-05 | 8.4 | 21.2 |
| Steam Tunnel | 23.26643 | 23.26643 | 23.26643 | 0.584 | 0.002061 | 0.288565 | | 1.71765E-06 | | |
| Miscellaneous | 0.356638 | 0.356638 | 0.356638 | 7.97744 | 0.028156 | 3.941794 | | 2.34631E-05 | | . · |
| TOTAL | 205.2 | 205.2 | 205.2 | 25.7 | 0.1 | 12.7 | 122.5 | 0.0 | 8.4 | 21.2 |

* Sourcewide VOC, Single HAP, and Total HAP PTE limited by annual towel processing limit, a synthetic minor limit

| | PTE After Modification (After Enforceable Limits) | | | | | | | | | |
|-----------------------------|---|----------|----------|---------|----------|----------|-------|-------------|------------------------|------------|
| Process or Emission Unit | PM | PM10 | PM2.5 | NOx | SO2 | со | VOC* | Lead | Highest Single HAP* | Total HAP* |
| Boiler B01 | 0.341365 | 0.341365 | 0.341365 | 7.6358 | 0.02695 | 3.772984 | | 2.24582E-05 | | |
| Process P01 | 0 | 0 | 0_ | 0 | 0 | 0 | | 0 | 8.4 2 | |
| Process P02 | 9.984731 | 9.984731 | 9.984731 | 0 | 0 | 0_ | 122.5 | 0 | | 21.2 |
| Process P03 | 157.487 | 157.487 | 157.487 | 8.03 | 0.028341 | 3.967765 | 122.5 | 2.36176E-05 | | |
| Steam Tunnel | 27.23322 | 27.23322 | 27.23322 | 2.19 | 0.007729 | 1.082118 | : | 6.44118E-06 | | |
| Miscellaneous | 0.356638 | 0.356638 | 0.356638 | 7.97744 | 0.028156 | 3.941794 | | 2.34631E-05 | | |
| TOTAL | 195.4 | 195.4 | 195.4 | 25.8 | 0.1 | 12.8 | 122.5 | 0.0 | 8.4 | 21.2 |

^{*} Sourcewide VOC, Single HAP, and Total HAP PTE limited by annual towel processing limit, a synthetic minor limit

| GHG Overview for G&K Services, Inc Green Bay | | | | | | | |
|--|----------|----------|----------|----------|--|--|--|
| CO2 CH4 N2O CO2e | | | | | | | |
| Before Modification | 18373.22 | 0.346273 | 0.034627 | 18392.2 | | | |
| After Modification | 18475.7 | 0.348204 | 0.03482 | 18494.78 | | | |

GK Services--Green Bay Statement of Basis - Calculations

Pollutant Potential to Emit Calculations and Methodology - Boiler B01

| | Heat Input | |
|---------------------------|------------|-------------|
| Emission Unit | Rate | Units |
| B01 | 10.46 | MMBTU/hr |
| Natural Gas Heating Value | 1020 | MMBTU/MMSCF |

| | Potential NG |
|------------|--------------|
| | Throughput |
| Unit | MMSCF/yr |
| Boiler B01 | 89.83294118 |

| Pollutant PTE - Combustion | | | | | | | | |
|--------------------------------|-----------|-------------|-----------|--------|-------------|---------|----------|-------------|
| | PM | PM10 | PM2.5 | NOx | SO2 | со | VOC | Lead |
| Pollutant Emission Factor | | | | | | | | |
| lb/MMSCF | 7.6 | 7.6 | 7.6 | 170 | 0.6 | 84 | 5.5 | 0.0005 |
| Potential Emissions in tons/yr | 0.3413652 | 0.341365176 | 0.3413652 | 7.6358 | 0.026949882 | 3.77298 | 0.247041 | 2.24582E-05 |

| HAP PTE - Combustion | | | | | | | | | |
|------------------------------|----------|-----------------|-------------|----------|----------|----------|--|--|--|
| Pollutant | Benzene | Dicholrobenzene | Formaldehyo | Hexane | Toluene | Total | | | |
| Pollutant Emission Factor | | | | | | | | | |
| lb/MMSCF | 2.10E-03 | 1.20E-03 | 7.50E-02 | 1.80E+00 | 3.40E-03 | 1.88E+00 | | | |
| Potential to Emit in tons/yr | 9.43E-05 | 5.39E-05 | 3.37E-03 | 8.08E-02 | 1.53E-04 | 8.45E-02 | | | |

Notes

MMBTU = 1,000,000 British Thermal Units, MMSCF = 1,000,000 standard cubic feet of natural gas

All PTE emissions assumed to be produced from combustion of natural gas.

Potential NG Throughput (MMSCF/yr) = Heat Input Capacity (MMBTU/hr) x 8760 hours/yr x 1 MMSCF / 1020 MMBTU

PTE (tons/yr) = Potential NG Throughput (MMSCF/yr) x Emission Factor (lb/MMSCF) / 2000 lbs/ton

Combustion emission factors are from AP-42, Volume 1, Fifth Edition, Chapter 1.4, Tables 1.4-1 and 1.4-2.

HAP emission factors are from AP-42, Chapter 1.4, Tables 1.4-3.

5 Highest HAPs are displayed for calculation purposes.

Pollutant Potential to Emit Calculations and Methodology - Process P01

| Shop Towel Feed Rate | |
|----------------------|----------|
| (lbs/hr) | 4688 |
| Shop Towel Feed Rate | |
| (1000 lbs/yr) | 41066.88 |

| Shop Towel | |
|------------|-----|
| Wash Time | 70% |

| | Shop Towel | Process P01 |
|------------------------|-----------------|-------------|
| | Emission Factor | PTE |
| Pollutant | (lb/1000 lb) | (tons/yr) |
| VOC | 12 | 172.480896 |
| 1,2-Dichloroethane | 0.04 | 0.57493632 |
| Cumene | 0.01 | 0.14373408 |
| Ethylbenzene | 0.07 | 1.00613856 |
| Methanol | 0.05 | 0.7186704 |
| Methyl Isobutyl Ketone | 0.06 | 0.86240448 |
| Methylene Chloride | 0.01 | 0.14373408 |
| Napthalene | 0.01 | 0.14373408 |
| n-Hexane | 0.005 | 0.07186704 |
| Tetrachloroethene | 1.75 | 25.153464 |
| Toluene | 1.55 | 22.2787824 |
| Trichloroethene | 0.21 | 3.01841568 |
| Xylene | | |
| (isomers and mixture) | 0.78 | 11.21125824 |
| m-Xylene | 0.355 | 5.10255984 |
| o-Xylene | 0.07 | 1.00613856 |
| p-Xylene | 0.355 | 5.10255984 |
| Total HAP | 4.545 | 65.32713936 |

Notes

Process P01 has a maximum feed rate of 4,688 pounds of soiled towels per hour.

Process P01 is not designed to wash soiled shop towels. Therefore, only shop towel PTE is considered in calculations.

Shop towel emission factors are based on source-specific testing and combines both washing and drying time. Shop towels spend 70% of the time in the washing process.

Process P01 contains only washing machines. Therefore, drying emissions are excluded.

Shop Towel Feed Rate (1000 lb/yr) = feed rate (lbs/hr) * 8760 (hr/yr) / 1000

PTE = feed rate (1000 lb/yr) * emission factor (lb/1000 lb) * 0.7/2000 (lb/ton)

Feed rate assumes that all units within this process are operated at their maximum load capacity. In actual practice, this may not occur.

Pollutant Potential to Emit Calculations and Methodology - Process P02

| | Print Towel | Shop Towel |
|-------------------------|-------------|------------|
| | | |
| Feed Rate (lbs/hr) | 2240 | 2600 |
| Feed Rate (1000 lbs/yr) | 19622.4 | 22776 |

| | Print | | Shop | |
|------------|-------|-----|------|-----|
| Cycle Time | | | | |
| (%) | | 95% | | 70% |

| | | | | Calculated | |
|---------------|---------------|------------|-------|------------|-------------|
| | | Stack Flow | Stack | Emission | |
| | Emission Rate | Rate | Temp | Factor | PM PTE |
| Emission Unit | (gr/dscf) | (acfm) | (°F) | (lb/hr) | (tons/yr) |
| Jensen #1 | 0.1 | 680 | 80 | 0.5699048 | 2.496182857 |
| Jensen #2 | 0.1 | 680 | 80 | 0.5699048 | 2.496182857 |
| Unimac #2 | 0.1 | 680 | 80 | 0.5699048 | 2.496182857 |
| Unimac #3 | 0.1 | 680 | 80 | 0.5699048 | 2.496182857 |
| Total | | | | | 9.984731429 |

| | Print Towel | Shop Towal | Print | | PTE |
|----------------------------|--------------|--------------|-----------|------------|------------------|
| | | Shop Towel | | Clara Tana | |
| | Emission | Emission | Towel | Shop Towel | Max of Print and |
| Pollutants measured during | | Factors | PTE | PTE | Shop Towels |
| stack test | (lb/1000 lb) | (lb/1000 lb) | (tons/yr) | (tons/yr) | (tons/yr) |
| voc | 127 | 12 | 1183.721 | 95.6592 | 1183.72128 |
| 1,2-Dichloroethane | 0.01 | 0.04 | 0.093206 | 0.318864 | 0.318864 |
| Cumene | 0.48 | 0.01 | 4.473907 | 0.079716 | 4.4739072 |
| Ethylbenzene | 1.88 | 0.07 | 17.5228 | 0.558012 | 17.5228032 |
| Methanol | 0.56 | 0.05 | 5.219558 | 0.39858 | 5.2195584 |
| Methyl Isobutyl Ketone | 0.24 | 0.06 | 2.236954 | 0.478296 | 2.2369536 |
| Methylene Chloride | 0.05 | 0.01 | 0.466032 | 0.079716 | 0.466032 |
| Napthalene | 0.01 | 0.01 | 0.093206 | 0.079716 | 0.0932064 |
| n-Hexane | 0.07 | 0.005 | 0.652445 | 0.039858 | 0.6524448 |
| Tetrachloroethene | 0.14 | 1.75 | 1.30489 | 13.9503 | 13.9503 |
| Toluene | 8.78 | 1.55 | 81.83522 | 12.35598 | 81.8352192 |
| Trichloroethene | 0.25 | 0.21 | 2.33016 | 1.674036 | 2.33016 |
| Xylene | | | | | |
| (isomers and mixture) | 6.32 | 0.78 | 58.90644 | 6.217848 | 58.9064448 |
| m-Xylene | 2.53 | 0.355 | 23.58122 | 2.829918 | 23.5812192 |
| o-Xylene | 1.26 | 0.07 | 11.74401 | 0.558012 | 11.7440064 |
| p-Xylene | 2.53 | 0.355 | 23.58122 | 2.829918 | 23.5812192 |
| Total HAP | 18.79 | 4.545 | 175.1348 | 36.230922 | 175.1348256 |

Notes:

Proces PO2 contains only washers. Therefore, only washing emissions are considered.

PM EF (lb/hr) = emission rate (gr/dscf) * 60 min/hr * (460 + 68) / (460 + Stack Temp °F) / 7000 gr/lb

PM PTE (tons/yr) = Emission Factor (lb/hr) * 8760 (hr/yr) / 2000 (lb/ton)

Based on best information available, PM10 and PM2.5 PTE are the same as PM PTE.

HAP & VOC PTE (tons/yr) = Emission factor (lb/1000 lb) * Feed Rate (lb/1000 lb) * cycle time (%) / 2000

Facility PTE is based on the maximum of either print towel PTE or shop towel PTE.

The units within this process group do not combust natural gas.

Feed rate assumes that all units within this process are operated at their maximum load capacity. In actual practice, this may not occur.

Pollutant Potential to Emit Calculations and Methodology - Process P03

| | Print Towel | Shop Towel |
|-------------------------|-------------|------------|
| Feed Rate (lbs/hr) | 5500 | 5340 |
| Feed Rate (1000 lbs/yr) | 48180 | 46778.4 |

| | Before Modification | After Modification |
|-------------------------|---------------------|--------------------|
| Total Heat Input Rate | | |
| (MMBTU/hr) | 13 | 11 |
| Potential NG Throughput | | |
| (MMSCF/yr) | 111.6470588 | 94.47058824 |

| | Print | Shop |
|------------|-------|------|
| Cycle Time | | |
| (%) | 5% | 30% |

| Natural Gas Heating | |
|---------------------|------|
| Factor | |
| (MMBTU/MMSCF) | 1020 |

| | | | Pollutant P | TE - Combustion | | | | |
|----------------------|-------------|-------------|-------------|-----------------|-------------|-------------|-------------|---------|
| | PM | PM10 | PM2.5 | NOx | SO2 | co | VOC | Lead_ |
| Natural Gas Emission | | 7 | | | 1 | | 1 | |
| Factors (lb/MMSCF) | 7.6 | 7.6 | 7.6 | 170 | 0.6 | 84 | 5.5 | 0.000 |
| Potential Emissions | | | | | | | | |
| Before Modification | | | | | | | | |
| (tons/yr) | 0.424258824 | 0.424258824 | 0.424258824 | 9.49 | 0.033494118 | 4.689176471 | 0.307029412 | 2.79E-0 |
| Potential Emissions | | | | | | | | |
| After Modification | Ì | İ | Ì | | 1 | | 1 | ł |
| (tons/yr) | 0.358988235 | 0.358988235 | 0.358988235 | 8.03 | 0.028341176 | 3.967764706 | 0.259794118 | 2.36E-0 |

| | | HAP PTE - | Combustion | | | |
|---------------------------|----------|-----------------|--------------|----------|----------|----------|
| Pollutant | Benzene | Dicholrobenzene | Formaldehyde | Hexane | Toluene | Total |
| Pollutant Emission Factor | İ | | | | | |
| Ib/MMSCF | 2.10E-03 | 1.20E-03 | 7.50E-02 | 1.80E+00 | 3.40E-03 | 1.88E+00 |
| Potential Emissions | | | | | | |
| Before Modification | | | | | | |
| (tons/yr) | 1.17E-04 | 6.70E-05 | 4.19E-03 | 1.00E-01 | 1.90E-04 | 1.05E-01 |
| Potential Emissions | | |] | | | |
| After Modification | | | [| [| | ĺ |
| (tons/yr) | 9.92E-05 | 5.67E-05 | 3.54E-03 | 8.50E-02 | 1.61E-04 | 8.89E-02 |

| | PM | PTE - Other Than Com | bustion | | |
|---------------------------|---------------|----------------------|------------|-----------------|-------------|
| | Emission Rate | Stack Flow Rate | Stack Temp | Emission Factor | PM PTE |
| Emission Unit | (gr/dscf) | (acfm) | (°F) | (lb/hr) | (tons/yr) |
| Cissell #1 | 0.1 | 2160 | 136 | 1.640191755 | 7.184039885 |
| Cissell #2 | 0.1 | 2160 | 136 | 1.640191755 | 7.18403988 |
| Challenge #3 | 0.1 | 9000 | 110 | 7.145864662 | 31.2988872 |
| Challenge #4 | 0.1 | 9000 | 110 | 7.145864662 | 31.2988872 |
| American #1 | 0.1 | 13500 | 110 | 10.71879699 | 46.94833083 |
| American #2 | 0.1 | 13500 | 110 | 10.71879699 | 46.9483308 |
| Jensen L-Tron Dryer #1 | 0.1 | 12000 | 120 | 9.363546798 | 41.01233498 |
| Jensen L-Tron Dryer #2 | 0.1 | 12000 | 120 | 9.363546798 | 41.01233498 |
| WashTech DR-80 Dryer | 0.1 | 1600 | 136 | 1.214956855 | 5.32151102 |
| Total Before Modification | | | | | 170.8625159 |
| Total After Modification | | | | | 157.1279953 |

| ·· | Combustion (tons/yr) | Other Than Combustion (tons/yr) | PM PTE |
|-------------------------|----------------------|---------------------------------------|-------------|
| PM PTE - Combustion and | | | |
| Other Sources | | | |
| Before Modification | 0.424258824 | 170.8625159 | 171.2867747 |
| PM PTE - Combustion and | | | |
| Other Sources | 1 | | |
| After Modification | 0.358988235 | 157.1279953 | 157.4869835 |

| | | | | | PTE | PTE | |
|----------------------------|------------------|------------------|-----------|------------|--------------|--------------|--------------------|
| | | | | | Max of Print | Before | PTE |
| | | | | Shop Towel | and Shop | Modification | After Modification |
| Pollutants Measured During | Emission Factors | Emission Factors | PTE | PTE | Towels | (Towel and | (Towel and |
| Stack Test | (lb/1000 lb) | (lb/1000 lb) | (tons/yr) | (tons/yr) | (tons/yr) | Combustion) | Combustion) |
| VOC | 127 | 12 | 152.9715 | 84.20112 | 152.9715 | 153.2785 | 153.2313 |
| 1,2-Dichloroethane | 0.01 | 0.04 | 0.012045 | 0.2806704 | 0.2806704 | 0.2807 | 0.2807 |
| Cumene | 0.48 | 0.01 | 0.57816 | 0.0701676 | 0.57816 | 0.5782 | 0.5782 |
| Ethylbenzene | 1.88 | 0.07 | 2.26446 | 0.4911732 | 2.26446 | 2.2645 | 2.2645 |
| Methanol | 0.56 | 0.05 | 0.67452 | 0.350838 | 0.67452 | 0.6745 | 0.6745 |
| Methyl Isobutyl Ketone | 0.24 | 0.06 | 0.28908 | 0.4210056 | 0.4210056 | 0.4210 | 0.4210 |
| Methylene Chloride | 0.05 | 0.01 | 0.060225 | 0.0701676 | 0.0701676 | 0.0702 | 0.0702 |
| Napthalene | 0.01 | 0.01 | 0.012045 | 0.0701676 | 0.0701676 | 0.0702 | 0.0702 |
| n-Hexane | 0.07 | 0.005 | 0.084315 | 0.0350838 | 0.084315 | 0.1848 | 0.1693 |
| Tetrachloroethene | 0.14 | 1.75 | 0.16863 | 12.27933 | 12.27933 | 12.2793 | 12.2793 |
| Toluene | 8.78 | 1.55 | 10.57551 | 10.875978 | 10.875978 | 10.8762 | 10.8761 |
| Trichloroethene | 0.25 | 0.21 | 0.301125 | 1.4735196 | 1.4735196 | 1.4735 | 1.4735 |
| Xylene | | | | | | | |
| (isomers and mixture) | 6.32 | 0.78 | 7.61244 | 5.4730728 | 7.61244 | 7.6124 | 7.6124 |
| m-Xylene | 2.53 | 0.355 | 3.047385 | 2.4909498 | 3.047385 | 3.0474 | 3.0474 |
| o-Xylene | 1.26 | 0.07 | 1.51767 | 0.4911732 | 1.51767 | 1.5177 | 1.5177 |
| p-Xylene | 2.53 | 0.355 | 3.047385 | 2.4909498 | 3.047385 | 3.0474 | 3.0474 |
| Total HAP | 18.79 | 4.545 | 22.632555 | 31.8911742 | 31.8911742 | 31.9918 | 31.9764 |

Notes: $PM \ EF \ (lb/hr) = emission \ rate \ (gr/dscf) * 60 \ min/hr * (460 + 68) / (460 + 5tack \ Temp *F) / 7000 \ gr/lb \\ PM \ PTE \ (tons/yr) = Emission \ Factor \ (lb/hr) * 8760 \ (hr/yr) / 2000 \ (lb/ton) \\ HAP \& VOC \ PTE \ (tons/yr) = Emission \ factor \ (lb/1000 \ lb) * Feed \ Rate \ (lb/1000 \ lb) * cycle time \ (%) / 2000 \\ Facility \ PTE \ is based on the maximum of either print towel \ PTE \ or shop towel \ PTE.$

Feed rate assumes that all units within this process are operated at their maximum load capacity. In actual practice, this may not occur. Combustion emission factors are from AP-42, Volume 1, Fifth Edition, Chapter 1.4, Tables 1.4-1 and 1.4-2.

Pollutant Potential to Emit Calculations and Methodology - Steam Tunnels

| | Heat Input |
|------------------------------|------------|
| Emission Unit | (MMBTU/hr) |
| Leonard 24-foot Steam Tunnel | 0.8 |
| Leonard VPT24 Steam Tunnel | 3 |

| | * | Heat Input | |
|---------------------------|---|------------|-------------|
| | | Rate | |
| Emission Unit | | | Units |
| Existing: 24-foot | | 0.8 | MMBTU/hr |
| Replacement: VPT24 | | 3 | MMBTU/hr |
| Natural Gas Heating Value | | 1020 | MMBTU/MMSCF |

| | Potential NG |
|--------------------|--------------|
| | Throughput |
| Unit | MMSCF/yr |
| Existing: 24-foot | 6.870588235 |
| Replacement: VPT24 | 25.76470588 |

| Pollutant PTE - Combustion | | | | | | | | |
|------------------------------------|-------------|-------------|------------|-------|-------------|---------|----------|----------|
| | PM | PM10 | PM2.5 | NOx | SO2 | со | voc | Lead |
| Pollutant Emission Factor | | | | | | | | |
| lb/MMSCF | 7.6 | 7.6 | 7.6 | 170 | 0.6 | 84 | 5.5 | 0.0005 |
| | | | | | | | | |
| PTE Before Modification in tons/yr | 0.026108235 | 0.026108235 | 0.02610824 | 0.584 | 0.002061176 | 0.28856 | 0.018894 | 1.72E-06 |
| | | | | | | | | |
| PTE After Modification in tons/yr | 0.097905882 | 0.097905882 | 0.09790588 | 2.19 | 0.007729412 | 1.08212 | 0.070853 | 6.44E-06 |

| HAP PTE - Combustion | | | | | | | | | |
|------------------------------------|----------|-----------------|-------------|----------|----------|----------|--|--|--|
| Pollutant | Benzene | Dicholrobenzene | Formaldehyd | Hexane | Toluene | Total | | | |
| Pollutant Emission Factor | | | | | | | | | |
| lb/MMSCF | 2.10E-03 | 1.20E-03 | 7.50E-02 | 1.80E+00 | 3.40E-03 | 1.88E+00 | | | |
| PTE Before Modification in tons/yr | 7.21E-06 | 4.12E-06 | 2.58E-04 | 6.18E-03 | 1.17E-05 | 6.46E-03 | | | |
| PTE After Modification in tons/yr | 2.71E-05 | 1.55E-05 | 9.66E-04 | 2.32E-02 | 4.38E-05 | 2.42E-02 | | | |

| | PM PTE - Other Than Combustion | | | | | | | |
|----------------------------------|--|---------------------------|--------------------|----------------------------|---------------------|--|--|--|
| Emission Unit | Emission Rate (gr/dscf) | Stack Flow Rate (acfm) | Stack Temp (°F) | Emission Factor (lb/hr) | PM PTE (tons/yr) | | | |
| Leonard 24-foot Steam Tunnel - | - | | | | | | | |
| Exh | 0.1 | 6800 | 120 | 5.306009852 | 23.24032315 | | | |
| Leonard VPT24 Steam Tunnel - Exh | | | | | | | | |
| 1 | 0.1 | 3790 | 120 | 2.957320197 | 12.95306246 | | | |
| Leonard VPT24 Steam Tunnel - Exh | | | | | | | | |
| 2 | 0.1 | 3790 | 120 | 2.957320197 | 12.95306246 | | | |
| Leonard VPT24 Steam Tunnel - | | | | | | | | |
| Combustion Unit | 0.1 | 471.27 | 300 | 0.28063597 | 1.229185548 | | | |
| TOTAL for VPT24 | en jagen en jagen en jagen en jagen en jagen en jagen en jagen en jagen en jagen en jagen en jagen en jagen en | | | | 27.13531047 | | | |

Total PM PTE, 24-foot Steam

Tunnel)

23.26643139

Total PM PTE, VPT24

27.23321636

Notes

MMBTU = 1,000,000 British Thermal Units, MMSCF = 1,000,000 standard cubic feet of natural gas

All PTE emissions assumed to be produced from combustion of natural gas.

Potential NG Throughput (MMSCF/yr) = Heat Input Capacity (MMBTU/hr) x 8760 hours/yr x 1 MMSCF / 1020 MMBTU

PTE (tons/yr) = Potential NG Throughput (MMSCF/yr) x Emission Factor (lb/MMSCF) / 2000 lbs/ton

 $Combustion\ emission\ factors\ are\ from\ AP-42,\ Volume\ 1,\ Fifth\ Edition,\ Chapter\ 1.4,\ Tables\ 1.4-1\ and\ 1.4-2.$

HAP emission factors are from AP-42, Chapter 1.4, Tables 1.4-3.

5 Highest Combustion HAPs are displayed for calculation purposes.

PM EF (lb/hr) = emission rate (gr/dscf) * 60 min/hr * (460 + 68) / (460 + Stack Temp °F) / 7000 gr/lb

PM PTE (tons/yr) = Emission Factor (ib/hr) * 8760 (hr/yr) / 2000 (lb/ton)

HAP emissions are assumed to only come from natural gas combustion since most of the HAPs are removed from the washed towels during the laundering process.

Pollutant Potential to Emit Calculations and Methodology - Miscellaneous Natural Gas Emission units

| | Heat Input |
|-----------------------------|------------|
| Émission Unit | (BTU/hr) |
| Gas Fired Unit Heater #1 | 150,000 |
| Gas Fired Unit Heater #2 | 150000 |
| Gas Fired Unit Heater #3 | 75000 |
| Gas Fired Unit Heater #4 | 165000 |
| Gas Fired Unit Heater #5 | 165000 |
| Gas Fired Unit Heater #6 | 105000 |
| Gas Fired Unit Heater #7 | 105000 |
| Gas Fired Unit Heater #8 | 1255000 |
| HVAC Units #1 | 250000 |
| HVAC Units #2 | 250000 |
| HVAC Units #3 | 205000 |
| MUA Units Roof #1 | 3575000 |
| MUA Units Roof #2 | 3575000 |
| MUA Units Roof #3 | 865000 |
| Convenience Water Heater #1 | 38000 |
| TOTAL | 10,928,000 |
| | |
| Total (MMBTU/hr) | 10.928 |

| | Heat Input | |
|---------------------------|------------|-------------|
| Emission Unit | Rate | Units |
| Total | 10.928 | MMBTU/hr |
| Natural Gas Heating Value | 1020 | MMBTU/MMSCF |

| | Potential NG |
|-------|--------------|
| | Throughput |
| Unit | MMSCF/yr |
| Total | 93.85223529 |

| Pollutant PTE - Combustion | | | | | | | | |
|-----------------------------------|-----------|-------------|-----------|---------|-------------|---------|----------|----------|
| PM PM10 PM2.5 NOx SO2 CO VOC Lead | | | | | | | | |
| Pollutant Emission Factor | | | | | | | | |
| lb/MMSCF | 7.6 | 7.6 | 7.6 | 170 | 0.6 | 84 | 5.5 | 0.0005 |
| Potential Emissions in tons/yr | 0.3566385 | 0.356638494 | 0.3566385 | 7.97744 | 0.028155671 | 3.94179 | 0.258094 | 2.35E-05 |

| HAP PTE | | | | | | | | |
|------------------------------|----------|-----------------|-------------|----------|----------|----------|--|--|
| Pollutant | Benzene | Dicholrobenzene | Formaldehyd | Hexane | Toluene | Total | | |
| Pollutant Emission Factor | | | | | | | | |
| lb/MMSCF | 2.10E-03 | 1.20E-03 | 7.50E-02 | 1.80E+00 | 3.40E-03 | 1.88E+00 | | |
| Potential to Emit in tons/yr | 9.85E-05 | 5.63E-05 | 3.52E-03 | 8.45E-02 | 1.60E-04 | 8.83E-02 | | |

Notes

 $\mathsf{MMBTU} = 1,\!000,\!000 \; \mathsf{British} \; \mathsf{Thermal} \; \mathsf{Units}, \; \mathsf{MMSCF} = 1,\!000,\!000 \; \mathsf{standard} \; \mathsf{cubic} \; \mathsf{feet} \; \mathsf{of} \; \mathsf{natural} \; \mathsf{gas}$

All PTE emissions assumed to be produced from combustion of natural gas. $% \label{eq:ptemp} % \label{eq:pt$

Potential NG Throughput (MMSCF/yr) = Heat input Capacity (MMBTU/hr) x 8760 hours/yr x 1 MMSCF / 1020 MMBTU

PTE (tons/yr) = Potential NG Throughput (MMSCF/yr) x Emission Factor (lb/MMSCF) / 2000 lbs/ton

Combustion emission factors are from AP-42, Volume 1, Fifth Edition, Chapter 1.4, Tables 1.4-1 and 1.4-2.

HAP emission factors are from AP-42, Chapter 1.4, Tables 1.4-3.

5 Highest HAPs are displayed for calculation purposes.

| | Capacity | Capacity |
|--------------------------------|-----------------------|----------------------|
| | (Before Modification) | (After Modification) |
| Natural Gas Combustion Sources | [MMBTU/hr] | [MMBTU/hr] |
| Boiler B01 | 10.46 | 10.46 |
| Cissel #1 | 0.25 | 0 |
| Cissel #2 | 0.25 | 0.25 |
| Challenge #3 | 2.75 | 2.75 |
| Challenge #4 | 2.75 | 2.75 |
| American #1 | 3.5 | 0 |
| American #2 | 3.5 | 0 |
| Jensen L-Tron Dryer #1 | 0 | 2.5 |
| Jensen L-Tron Dryer #2 | 0 | 2.5 |
| WashTech DR-80 Dryer | 0 | 0.25 |
| Leondard 24-foot Steam Tunnel | 0.8 | 0 |
| 3 MMBTU/hr Tunnel Replacement | 0 | 3 |
| Insignificant Activities | 11.6 | 11.6 |
| TOTAL | 35.86 | 36.06 |

| (Before Modification) | Greenhouse Gas PTE | | | | | |
|---------------------------------|--------------------|-------------|----------|--|--|--|
| GHG Species | CO2 | CH4 | N2O | | | |
| Emission Factor in kg/MMBTU | 53.06 | 1.00E-03 | 1.00E-04 | | | |
| Potential Emission in tons/yr | 18373.22461 | 3.46E-01 | 3.46E-02 | | | |
| Global Warming Potential | 1 | 25 | 298 | | | |
| CO2e Per GHG Species in tons/yr | 18373.22461 | 8.656815215 | 10.31892 | | | |
| Total Potential CO2e in tons/yr | 18392.20035 | | | | | |

| (After Modification) | Greenhouse Gas PTE | | | | | |
|---------------------------------|--------------------|-------------|-----|-------------|----------|--|
| GHG Species | CO2 | | CH4 | | N2O | |
| Emission Factor in kg/MMBTU | | 53.06 | | 1.00E-03 | 1.00E-04 | |
| Potential Emission in tons/yr | | 18475.69659 | | 3.48E-01 | 3.48E-02 | |
| Global Warming Potential | | 1 | | 25 | 298 | |
| CO2e Per GHG Species in tons/yr | | 18475.69659 | | 8.705096393 | 10.37647 | |
| Total Potential CO2e in tons/yr | | 18494.77816 | | | | |

Notes

1 MMBTU = 1,000,000 British Thermal Units

GHG PTE (tons/yr) = Heat Input Capacity (MMBTU/hr) x 8760 hr/yr x Emission Factor (kg/MMBTU) x 2.20462 lb/kg / 2000 lbs/ton CO2e (tons/yr) = CO2 PTE (tons/yr) x CO2 GWP (1) + CH4 PTE (tons/yr) x CH4 GWP (21) + N2O PTE (tons/yr) x N2O GWP (310) GHG Emission Factors and GWP from 40 CFR 98, Table A-1, C-1, and C-2 for natural gas combustion.

GHG Values based on November 29, 2013, GWP and Default Values